Trimming the Iterative Fat of Equilibrium Thermodynamic Models Using Neural Networks

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 Iterative solvers can be computationally expensive.

Typical approach



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- But, they are transparent and scientifically robust.
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- But, they are transparent and scientifically robust.
- Neural networks are the ultimate black box.
- But, they can be faster than iterative solvers.
- A combined approach is preferable.

Typical approach Guess $\longrightarrow \bigcirc 0$ Obj. $\downarrow \frown \bigcirc$



Modeling aerosol mass concentrations²







water vapor equil.

Modeling aerosol mass concentrations²



Modified Raoult's law

- Mixing decreases the effective vapor pressure of each component.
- $\square p_j = p_j^{\text{sat}} x_j \gamma_j = p_j^{\text{sat}} a_j$
- The activity coefficient (γ_j) parameterizes the energetic cost (favorability) of mixing.





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- In terms of an effective volatility.

$$\bullet C_j^* = C_j^{\text{sat}} C_{\Sigma_k}^{\Sigma_{\pi}} \frac{\gamma_j q_j^{\pi}}{M_j \sum_k \frac{C_k^2}{M_j}}$$

Unfavorable interactions





BAT: A reduced complexity model

 AIOMFAC is used as a high fidelity reference.

Multi-component mixture



Non-ideal interactions among all species

Gorkowski et al. (2019)

BAT: A reduced complexity model

- AIOMFAC is used as a high fidelity reference.
- A simpler Binary Activity Thermodynamics model is built using AIOMFAC generated data.
- github.com/Gorkowski/ Binary_Activity_ Thermodynamics_Model

Multi-component mixture



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Binary Activity Thermodynamics

BAT approximation



Non-ideal interactions with water

Gorkowski et al. (2019)

BAT: Essential equations

- Following a power series expansion of molar excess Gibbs energy of mixing (G^E) (Redlich and Kister, 1948).
- Generalized by parameterizing the expansion coefficients (*c_n*).

$$G^{E}/RT = \phi_{org}(1 - \phi_{org}) [c_{1} + c_{2}(1 - 2\phi_{org})] \quad (1)$$

$$c_{n} = a_{n,1} \exp(a_{n,2} \times \mathbf{O} : \mathbf{C}) + a_{n,3} \exp\left(a_{n,4} \frac{M_{w}}{M_{org}}\right) \quad (2)$$

BAT: Essential equations

C

- Following a power series expansion of molar excess Gibbs energy of mixing (G^E) (Redlich and Kister, 1948).
- Generalized by parameterizing the expansion coefficients (*c_n*).
- Dependent variables

% water activity ($a_w \times 100\% \approx RH$) and organic activity

$$G^{E}/RT = \phi_{org}(1 - \phi_{org}) [c_{1} + c_{2}(1 - 2\phi_{org})] \quad (1)$$

$$a_{n} = a_{n,1} \exp(a_{n,2} \times \mathbf{0} : \mathbf{C}) + a_{n,3} \exp\left(a_{n,4} \frac{M_{w}}{M_{org}}\right) \quad (2)$$

$$(2)$$

$$\ln(\gamma_w) = (G^E/RT) - x_{org} \frac{d(G^E/RT)}{dx_{org}}$$
(3)

$$a_w = \gamma_w (1 - x_{org}) \tag{4}$$

Gorkowski et al. (2019)

Inverting the BAT model

For gas–particle partitioning we need γ_j and $\mathbf{x}_{org,j}$; both are used in $C_j^* = C_j^{\text{sat}} C_{\Sigma_k}^{\Sigma_{\pi}} \frac{\gamma_j q_j^{\pi}}{M_j \sum_k \frac{C_k}{M_i}}$.

3-D Models will have:

- 0:C
- M_{org}
- **RH** $\approx a_w \times 100\%$

Inverting the BAT model

For gas–particle partitioning we need γ_j and $x_{org,j}$; both are used in $C_j^* = C_j^{\text{sat}} C_{\Sigma_k}^{\Sigma_{\pi}} \frac{\gamma_j q_j^{\alpha}}{M_j \sum_k \frac{C_{\pi}}{M_k}}$.

3-D Models will have:

- 0:C
- M_{org}
- **RH** $\approx a_w \times 100\%$

- BAT model must be inverted to use *a_w* as an input.
- Iterative refinement is possible by varying x_{org,j} to match a_w.
- Instead neural networks are used to directly predict x_{org,j} to a high degree of accuracy.

Building a Neural Network

- We used a deep belief network of artificial neurons.
- In effect this acts as a generalized curve fitting tool.
- A training database of random inputs and targeted outputs is generated with the BAT model.



Training of Neural Network



Training of Neural Network



Neural Networks in the context of BAT



Neural Networks in the context of BAT ⁹



Targeting 3-D models (GEOS-Chem)



Isoprene SOA: NN underpredicts

- MCM simulation outputs.
- Isoprene and O₃ at 100 ppb.
- Simulation of 343 products after 12 hr.
- Used the EVAPORATION model for vapor pressure estimations.



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- The errors in partitioning coefficients are not directly translated to PM mass errors.



$\alpha\text{-Pinene SOA: NN underpredicts}$

- α-Pinene and O₃ at 20 ppb.
- Simulation of 198 products after 12 hr.



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- NN+refinement was 2-5 times faster than iterative refinement only.



$\alpha\text{-Pinene SOA: NN underpredicts}$

- α -Pinene and O_3 at 20 ppb.
- Simulation of 198 products after 12 hr.
- NN only was 1.5x faster.
- NN+refinement was 2-5 times faster than iterative refinement only.



α -Pinene SOA: PM mass agrees well



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- Extensions to the BAT model will look at organic-organic and inorganic-organic equilibrium modeling.



Volatility is dependent on RH



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Volatility is dependent on RH











Water mass also agrees



Measurement agreement of organic mass fractions



Side note on Köhler curves of CCN



Measurement agreement: κ_{CCN}



30 comparison points
 Error of ±0.055

BAT sequels

Organic-organic interactions



Inorganic-organic interactions



2-Phase systems



Camilo is pursuing the implementation into GEOS-Chem.



0 3 7 11 15 PM organic mass (μg m⁻³)

Gorkowski, K., Preston, T. C., and Zuend, A.: RH-dependent organic aerosol thermodynamics via an efficient reduced-complexity model, Atmos. Chem. Phys. Discuss., pp. 1–37, https://doi.org/10.5194/acp-2019-495, URL https://www.atmos-chem-phys-discuss.net/acp-2019-495/, 2019.

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